

STATE LEVEL ENVIRONMENT IMPACT ASSESSMENT AUTHORITY

Environment department, Room No. 217, 2nd floor, Mantralaya, Annexe, Mumbai- 400 032. Date:May 7, 2019

To.

Deepak Fertilizers and Petrochemicals Corporation Limited at Plot No K1-K8, MIDC Taloja, Panvel

Environment Clearance for Proposed expansion of manufacturing of Iso Propyl Alcohol- Petroleum products and petrochemical based processing facility at Plot No K1-K8, MIDC Taloja, Panvel by Deepak Fertilizers and Petrochemicals Corporation Limited

Sir,

This has reference to your communication on the above mentioned subject. The proposal was considered as per the EIA Notification - 2006, by the State Level Expert Appraisal Committee-I, Maharashtra in its 159th (A) - Day-2th meeting and recommend the project for prior environmental clearance to SEIAA. Information submitted by you has been considered by State Level Environment Impact Assessment Authority in its 165th meetings.

2. It is noted that the proposal is considered by SEAC-I under screening category 5 (e)- B as per EIA Notification 2006.

Brief Information of the project submitted by you is as below:-

1.Name of Project	Proposed expansion of manufacturing of Iso Propyl Alcohol- Petroleum products and petrochemical based processing facility at Plot No K1-K8, MIDC Taloja, Panvel by Deepak Fertilizers and Petrochemicals Corporation Limited
2.Type of institution	Private
3.Name of Project Proponent	Deepak Fertilizers and Petrochemicals Corporation Limited
4.Name of Consultant	Aditya Environmental Services Private Limited
5.Type of project	Not applicable
6.New project/expansion in existing project/modernization/diversification in existing project	Expansion of existing project
7.If expansion/diversification, whether environmental clearance has been obtained for existing project	Yes. GIIIIGII UI
8.Location of the project	Plot No K1-K8, MIDC Taloja, Panvel
9.Taluka	Panvel
10.Village	Taloja
Correspondence Name:	Mr. Deepak Pande
Room Number:	
Floor:	
Building Name:	
Road/Street Name:	
Locality:	
City:	
11.Whether in Corporation / Municipal / other area	MIDC Taloja

SEIAA Meeting No: 165 Meeting Date: April 26, 2019 (SEIAA-STATEMENT-000000807) SEIAA-MINUTES-000001856 SEIAA-EC-0000001501 (Jan.

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MIDC approved plot plan				
IOD/IOA/Concession/Plan Approval Number: MIDC approved plot plan				
Approved Built-up Area: 270889				
Expansion within existing project.				
MIDC approved plot plan				
385584 sq m				
Not applicable				
Not applicable				
FSI area (sq. m.): Not applicable				
Non FSI area (sq. m.): Not applicable				
Total BUA area (sq. m.): 14050				
Approved FSI area (sq. m.): 306399				
Approved Non FSI area (sq. m.): NA				
Date of Approval: 28-08-2015				
Not applicable				
Not applicable				
8437500000				

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22.Production Details							
Serial Number	Product	Existing (MT/M)	Proposed (MT/M)	Total (MT/M)			
1	Liquid CO2	72,000 MT/A	0 MT/A	72,000 MT/A			
2	Ammonia	140,400 MT/A	0 MT/A	140,400 MT/A			
3	Methanol	99,996 MT/A	0 MT/A	99,996 MT/A			
4	Weak Nitric acid	445,500 MT/A	0 MT/A	445,500 MT/A			
5	Concentrated nitric acid	129,600 MT/A	0 MT/A	129,600 MT/A			
6	Multiple grade NPK Fertilizer	6,00,000 MT/A	525000 MT/A	11,25,000 MT/A			
7	Technical grade ammonium nitrate" plus ammonium nitrate melt	444,000 MT/A	0 MT/A	444,000 MT/A			
8	Iso propyl alcohol (IPA)	70200 MT/A	110000 MT/A	180200 MT/A			
9	Electric power	9.4 MW	0 MT/A	9.4 MW			
10	Steam	1,056 MT/day	0 MT/A	1,056 MT/day			
11	Bentonite sulphur pastilles	25,000 MT/A	0 MT/A	25,000 MT/A			
12	Iso propyl alcohol (for drum filling operation (packaging operation) only)	15,000 MT/A	0 MT/A	15,000 MT/A			
13	Di iso propyl ether (DIPE) (for drum filling operation (packaging operation) only	15000 MT/A	0 МТ/А	15000 MT/A			
14	Gas based power generation (excluding DG sets)	17.9 MW	0 MT/A	17.9 MW			
15	Propane (By product)	33,000 MT/A	15,000 MT/A	48,000 MT/A			
16	Calcium phosphate (By product)	210 MT/A	0 MT/A	210 MT/A			
17	Crude DIPE (By product)	1,440 MT/A	0 MT/A	1,440 MT/A			
18	Di iso propyl ether (DIPE) (By product)	0 MT/A	7000 MT/A	7000 MT/A			
19	Hydrogen gas (By product)	960 MT/A	0 MT/A	960 MT/A			
20	Crude IPA/NPA mixture (By product)	1,080 MT/A	1500 MT/A	2580 MT/A			

23.Total Water Requirement

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	Source of water	MIDC Taloja
	Fresh water (CMD):	23142 CMD
	Recycled water - Flushing (CMD):	Not applicable
	Recycled water - Gardening (CMD):	Not applicable
	Swimming pool make up (Cum):	Not applicable
Dry season:	Total Water Requirement (CMD):	23863 CMD (23142 CMD from MIDC and 721 CMD recycle)
	Fire fighting - Underground water tank(CMD):	Not applicable
	Fire fighting - Overhead water tank(CMD):	Not applicable
	Excess treated water	Not applicable
	Source of water	Not applicable
	Fresh water (CMD):	Not applicable
	Recycled water - Flushing (CMD):	Not applicable
	Recycled water - Gardening (CMD):	Not applicable
	Swimming pool make up (Cum):	Not applicable
Wet season:	Total Water Requirement (CMD):	Not applicable
	Fire fighting - Underground water tank(CMD):	Not applicable
	Fire fighting - Overhead water tank(CMD):	Not applicable
	Excess treated water	Not applicable
Details of Swimming pool (If any)	Not applicable	IIIIIGIIL UI

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		2	4.Detai	ls of Tot	al water o	consume	d			
Particula rs	Consumption (CMD)			Loss (CMD)		Effluent (CMD)				
Water Require ment	Existing	Proposed	Total	Existing	Proposed	Total	Existing	Proposed	Total	
Domestic	172	0	172	18.5	0	18.5	153.5	0	153.5	
Industrial Process	2358	480	2838	1188.7	130	1668.7	1169.3	350	1169.3	
Cooling tower & thermopa ck	18813	2040	20853	16004.02	1669	18044.02	2808.98	371	2808.98	
			77			7/7				
		Level of the		च्छेवर	त्राधिका		7			
		Size and no tank(s) and Quantity:	of RWH	- %		929				
		Location of tank(s):	the RWH	N 0 S	B.0.	A 3	E			
25.Rain V Harvestin	25.Rain Water		Quantity of recharge pits:							
(RWH)		Size of recharge pits :			· 发展					
		Budgetary allocation (Capital cost) :								
		Budgetary allocation (O & M cost):		7	Town well of the					
		Details of UGT tanks if any:		1	The same of the sa					
				411	HILLE	\sim				
26 Storm	water	Natural wat drainage pa								
26.Storm drainage	water	Quantity of storm water:			rnment of					
		Size of SWI):	Detailed of	Detailed drawing is attached as Annexure 6					
				_						
		Sewage ger in KLD:	eration	153.5 cm	153.5 cmd					
		STP techno	logy:	Sewage w	Sewage water is used as food to bacteria in bioreactor at ETP.					
27.Sewa	ne and	Capacity of (CMD):	STP							
Waste w		Location & the STP:	area of							
		Budgetary a (Capital cos	allocation st):	1						
		Budgetary a (O & M cost		1						

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28.Solie	d waste Management
Waste generation:	Ready mixed concrete will be used to avoid/minimise civil debris and dust emission. Also soil will be refilled back.
Disposal of the construction waste debris:	Scrap generated will be sold to recycler.
Dry waste:	
Wet waste:	
Hazardous waste:	Spent catalyst, Residue and wastes, Discarded containers/liners, Used oil filters (non-metallic), Residues and wastes (silica gel), Date expired, discarded and off specification drugs (Ni Cd batteries), Used/Spent oil, Waste/residue containing oil, Used containers, Spray cans, spent catalyst, Used denoxed catalyst as spent catalyst, ,Used oil filters (nonmetallic), Date expired, discarded and off specification drugs (Lead acid batteries), Date expired, discarded and off specification drugs (Dry
Biomedical waste (If applicable):	Soiled waste, Glassware
STP Sludge (Dry sludge):	- 3
Others if any:	
Dry waste:	
Wet waste:	
Hazardous waste:	Hazardous waste will be disposed of to CHWTSDF/ sale to authorized Recycler or Reuser as per Hazardous waste rule 2016.
Biomedical waste (If applicable):	Biomedical waste will be disposed off as per Biomedical waste rule 2016.
STP Sludge (Dry sludge):	
Others if any:	LANGE HELL AND LEAVEN TO
Location(s):	Within plot
Area for the storage of waste & other material:	ACCOUNTY OF THE PROPERTY OF TH
Area for machinery:	
Capital cost:	rnment ot
	Waste generation: Disposal of the construction waste debris: Dry waste: Wet waste: Hazardous waste: Biomedical waste (If applicable): STP Sludge (Dry sludge): Others if any: Dry waste: Wet waste: Hazardous waste (If applicable): STP Sludge (Dry sludge): Others if any: Location(s): Area for the storage of waste & other material: Area for machinery:

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		29.Effluent Charecterestics							
2		Parameters	Unit			Effluent discharge standards (MPCB)			
3 BOD mg/lit 200 - 300 < 100 < 100 4 TDS mg/lit 1000-1500 < 2100 < 2100 5 Ammonical nitrogen mg/lit 1800 - 2000 < 50 < 50 6 Nitrate nitrogen mg/lit 150 - 200 < 20 < 20 7 Phosphate mg/lit 80-100 < 5.0 < 5.0 8 Free Ammonical nitrogen mg/lit 100-150 < 4 < 4 9 Suspended solids mg/lit 70 - 80 < 100 < 100 Amount of effluent generation (CMD): 4131.78 + 721(from IPA expansion) = 4852.78 CMD Capacity of the ETP: 4200 CMD Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. Note on ETP technology to be used Note on ETP technology to be used Aeration tank > Sec. Clarifier II > Denitrification reactor II > RO > Permeate recycle, 2. Proposed: Ceramic based membranes , ion exchange resins followed by bioreactor Page 100 Page 100 Page 100 A	1	рН		- 4 - 9 6 - 8.5 6 - 8.5					
4 TDS mg/lit 1000-1500 < 2100 < 2100 5 Ammonical nitrogen mg/lit 1800 - 2000 < 50 < 50 6 Nitrate nitrogen mg/lit 150 - 200 < 20 < 20 7 Phosphate mg/lit 80-100 < 5.0 < 5.0 8 Free Ammonical nitrogen mg/lit 100-150 < 4 < 4 9 Suspended solids mg/lit 70 - 80 < 100 < 100 Amount of effluent generation (CMD): Capacity of the ETP: 4200 CMD Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. Note on ETP technology to be used Note of ETP technology to be used Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	2	Oil and grease	mg/lit	mg/lit 2 - 3 < 10 < 10					
5 Ammonical nitrogen mg/lit 1800 - 2000 < 50 < 50 6 Nitrate nitrogen mg/lit 150 - 200 < 20 < 20 7 Phosphate mg/lit 80-100 < 5.0 < 5.0 8 Free Ammonical nitrogen mg/lit 100-150 < 4 < 4 9 Suspended solids mg/lit 70 - 80 < 100 < 100 Amount of effluent generation (CMD): Capacity of the ETP: 4200 CMD Amount of treated effluent recycled: Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. Note on ETP technology to be used Note on ETP technology to be used Note on ETP technology to be used RO > Permeate recycle, 2. Proposed: Ceramic based membranes , ion exchange resins followed by bioreactor	3	BOD	mg/lit	200 - 300	< 100	< 100			
6 Nitrate nitrogen mg/lit 150 - 200 < 20 < 20 7 Phosphate mg/lit 80-100 < 5.0 < 5.0 8 Free Ammonical nitrogen mg/lit 100-150 < 4 < 4 9 Suspended solids mg/lit 70 - 80 < 100 < 100 Amount of effluent generation (CMD): Capacity of the ETP: 4200 CMD Amount of treated effluent recycled: Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. Note on ETP technology to be used Note on ETP technology to be used Permeater recycle, 2. Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	4	TDS	mg/lit	1000-1500	< 2100	< 2100			
7 Phosphate mg/lit 80-100 < 5.0 < 5.0 8 Free Ammonical nitrogen mg/lit 100-150 < 4 < 4 9 Suspended solids mg/lit 70 - 80 < 100 < 100 Amount of effluent generation (CMD): 4131.78 + 721(from IPA expansion) = 4852.78 CMD Capacity of the ETP: 4200 CMD Amount of treated effluent recycled: 721 CMD Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. Note on ETP technology to be used Permeate recycle, 2. Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	5	Ammonical nitrogen	mg/lit	1800 - 2000	< 50	< 50			
8 Free Ammonical nitrogen mg/lit 100-150 < 4 < 4 9 Suspended solids mg/lit 70 - 80 < 100 < 100 Amount of effluent generation (CMD): 4131.78 + 721(from IPA expansion) = 4852.78 CMD Capacity of the ETP: 4200 CMD Amount of treated effluent recycled: 721 CMD Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. 1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammonistripper > Denitrification reactor II > Sec. clarifier I > Denitrification reactor II > RO > Permeate recycle, 2. Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	6	Nitrate nitrogen	mg/lit	150 - 200	< 20	< 20			
9 Suspended solids mg/lit 70 - 80 <100 <100 Amount of effluent generation (CMD): 4131.78 + 721(from IPA expansion) = 4852.78 CMD Capacity of the ETP: 4200 CMD Amount of treated effluent recycled: 721 CMD Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. Note on ETP technology to be used 1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammonstripper > Denitrification reactor II > Aeration tank > Sec. clarifier I > Denitrification reactor II > RO > Permeate recycle, 2. Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	7	Phosphate	mg/lit	80-100	< 5.0	< 5.0			
Amount of effluent generation (CMD): Capacity of the ETP: 4200 CMD Amount of treated effluent recycled: Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. 1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammonistripper > Denitrification reactor I > Sec. clarifier I > Denitrification reactor II > Aeration tank > Sec. clarifier II > Final Polishing tank High TDS effluent stream > RO > Permeate recycle, 2. Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	8		mg/lit	100-150	< 4	< 4			
Capacity of the ETP: Amount of treated effluent recycled: Amount of water send to the CETP: Amount of water send to the CETP: Amount of water send to the CETP: 4200 CMD 721 CMD Yes. Unit is already member of CETP. 1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammonistripper > Denitrification reactor I > Sec. clarifier I > Denitrification reactor II > RO > Permeate recycle, 2. Proposed: Ceramic based membranes , ion exchange resins followed by bioreactor	9	Suspended solids	mg/lit	70 - 80	<100	<100			
Amount of treated effluent recycled: Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. 1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammon stripper > Denitrification reactor I > Sec. clarifier I > Denitrification reactor II > Aeration tank > Sec. clarifier II > Final Polishing tank High TDS effluent stream > RO > Permeate recycle, 2. Proposed: Ceramic based membranes , ion exchange resins followed by bioreactor		effluent generation	4131.78 + 3	721(from IPA expansion)	= 4852.78 CMD				
recycled: Amount of water send to the CETP: 4131.78 CMD Membership of CETP (if require): Yes. Unit is already member of CETP. 1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammonistripper > Denitrification reactor I > Sec. clarifier I > Denitrification reactor II > Aeration tank > Sec. clarifier II > Final Polishing tank High TDS effluent stream > RO > Permeate recycle, 2. Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	Capacity of	the ETP:	4200 CMD	مألم	301.				
Membership of CETP (if require): Yes. Unit is already member of CETP. 1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammons stripper > Denitrification reactor I > Sec. clarifier I > Denitrification reactor II > Aeration tank > Sec. clarifier II > Final Polishing tank High TDS effluent stream > RO > Permeate recycle, 2. Proposed: Ceramic based membranes , ion exchange resins followed by bioreactor	1	reated effluent	721 CMD	70 5	3				
1. Existing: Low TDS effluent stream > Collection tank > Reaction tank > Ammonistripper > Denitrification reactor I > Sec. clarifier I > Denitrification reactor II > Aeration tank > Sec. clarifier II > Final Polishing tank High TDS effluent stream > RO > Permeate recycle, 2. Proposed: Ceramic based membranes, ion exchange resins followed by bioreactor	Amount of v	water send to the CETP:	4131.78 CM	ID (I)	対にて				
Note on ETP technology to be used Stripper $>$ Denitrification reactor I $>$ Sec. clarifier I $>$ Denitrification reactor II $>$ Aeration tank $>$ Sec. clarifier II $>$ Final Polishing tank High TDS effluent stream $>$ RO $>$ Permeate recycle, 2. Proposed: Ceramic based membranes , ion exchange resins followed by bioreactor	Membershi	p of CETP (if require):	require): Yes. Unit is already member of CETP.						
Disposal of the ETP sludge	Note on ET	Note on ETP technology to be used Stripper $>$ Denitrification reactor I $>$ Sec. clarifier I $>$ Denitrification reactor II $>$ Aeration tank $>$ Sec. clarifier II $>$ Final Polishing tank High TDS effluent stream $>$ RO $>$ Permeate recycle, 2. Proposed: Ceramic based membranes, ion exchange							
	Disposal of	the ETP sludge	ETP sludge	will be sent to CHWTSD	F for landfill.				

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30.Hazardous Waste Details							
Serial Number	Description	Cat	UOM	Existing	Proposed	Total	Method of Disposal
1	Spent catalyst	18.1	MT/Y	48.34	210	258.34	Sale to authorized party approved by CPCB/ MPCB
2	Residue and wastes	31.1	MT/Y	10	115	125	Sale to recycler/ CHWTSDF
3	Discarded containers/liners	33.3	MT/Y	346	0	346	Sale to authorized party for decontamination
4	Used oil filters (non metallic)	5.2	No/Y	25	6	31	CHWTSDF
5	Residues and wastes (silica gel)	31.1	MT/2 years	60 MT/2 years	07	60 MT/2 years	Sale to authorized party / recycler
6	Date expired, discarded and off specification drugs (Ni Cd batteries)	28.3	once in 5 years	400 No once in 5 years	60 No once in 5 years	460 No once in 5 years	Sale to reuser
7	Used/ Spent oil	5.1	KL/Y	130	7 3	137	Sale to authorized party approved by CPCB/ MPCB
8	Waste/ residue containing oil	5.2	MT/Y	10	2	12	CHWTSDF
9	Used containers	33.3	No/Y	3012	0	3012	CHWTSDF
10	Spray cans	33.3	No/Y	900	200	1100	CHWTSDF
11	Platinum, Rhodium catalyst as spent catalyst	17.2	Kg/Y	100	0	100	CHWTSDF/sale to recycler
12	Used denoxed catalyst as spent catalyst	17.2	MT/6 years	10	0	10	CHWTSDF/sale to recycler
13	Used oil filters (nonmetallic)	5.2	No/Y	20	\mathcal{N}_0	20	CHWTSDF
14	Date expired, discarded and off specification drugs (Lead acid batteries)	28.3	No/Y	34	20	54	Sale to reuser
15	Date expired, discarded and off specification drugs (Dry cell batteries)	28.3	No/Y	300	50	350	Sale to reuser
16	Chemical sludge from waste water treatment	35.3	TPM	30	0	30	sent to CHWTSDF
17	Ion exchange resins	35.2	TPM	0	100	100	sent to CHWTSDF
31.Stacks emission Details							
Serial Number	Section & units	Fuel Us Qua		Stack No.	Height from ground level (m)	Internal diameter (m)	Temp. of Exhaust Gases
1	Ammonia Primary reformer (existing)	Natural Ga sm3	s - 94218.5 /day		30	1.373	170 deg C
2	Boiler A & B (existing)	Natural gas - 32400 sm MTPD	3/day or 50		30 (common stack)	1	125 deg C



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	1					
3	Methanol Primary reformer (Existing)	Natural Gas - 60150 sm3/day		30	1.373	115 deg C
4	CNA Plant 1 (Existing)			42	0.075	25 deg C
5	CNA Plant 2 (Existing)			42	0.075	25 deg C
6	CNA Plant 3 (Existing)			42	0.075	25 deg C
7	WNA-I Plants (Existing)			39	0.953	38 deg C
8	WNA II Plants (Existing)			39	0.953	38 deg C
9	WNA III Plants (Existing)	1		60	0.953	38 deg C
10	WNA IV Plants(Existing)	MATO	1(1)72	52	0.953	130 Deg C
11	ANP Prilling tower (Existing)	Mada	1 Step	84	1.5	50 Deg C
12	LDAN Prilling tower (Existing)	7:42	3/	84	1.3	50 Deg C
13	ANP cyclone separator (Existing)	- 20 m	200	30	1.5	34 Deg C
14	ANP vacuum pump(Existing)	F O ADS	30-	27.8	0.2	35 deg C
15	LDAN ventury scrubber(Existing)		學為	24.5	1.5	41 deg C
16	Boiler C (Standby) (Existing)	Natural Gas - 12600 sm3/day	.:	30.5		125 Deg C
17	Boiler D (Standby) (Existing)	Natural gas / FO – 54000 sm3/day or 40 MTPD		63	Ťm	170 Deg C
18	CES - A engine exhaust boiler(Existing)	Natural Gas - 30750 sm3/day	मुद्रा	30.75	1.5	205 deg C
19	CES - B engine exhaust boiler(Existing)	Natural Gas - 30750 sm3/day	W.	30.75	1.5	205 deg C
20	CO2 liquifier 1 (Existing)	Vorn	m	-8	0.025	24 Deg C
21	CO2 liquifier 2 (Existing)	V GIIII		8	0.025	24 Deg C
22	Stripper 1 (Existing)			5.1	0.511	-60 Deg C
23	Stripper 2 (Existing)	ahar	20	5.1	0.511	-60 Deg C
24	Combined (1 Nos) (Existing)	allal	a 3	8	0.075	122 Deg C
25	Turbine - 1 (Existing)	Natural Gas - 37120 sm3/day		30	1.067	125 Deg C
26	HRSG - 1(Existing)	Natural gas/ Naphtha - 19584 sm3/day or 30 MTPD		30	1.067	125 Deg C
27	Turbine - 2 (Existing)	Natural Gas - 37120 sm3/day		30	1.067	125 Deg C
28	HRSG - 2 (Existing)	Natural gas/ Naphtha - 19584 sm3/day or 30 MTPD		30	1.067	125 Deg C



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		Natural Gas - 42888				
29	Turbine - 3 (Existing)	sm3/day		30	1.5	550 Deg C
30	HRSG - 3 (Existing)			30	1.5	190 Deg C
31	Turbine - 4 Existing)	Natural Gas - 42888 sm3/day	-	30	1.5	550 Deg C
32	HRSG - 4(Existing)			30	1.5	190 Deg C
33	Turbine - 5 (Existing)	Natural Gas - 45984 sm3/day		30	1.5	550 Deg C
34	HRSG - 5 (Existing)			30	1.5	190 Deg C
35	G P Vent (Existing)			30	0.64	110 Deg C
36	780 weak nitric acid plant(Existing)		M	48	1.3	131 deg C
37	600 TPD LDAN prilling towers, dryers(Existing)	WI THE	Teron	27	1.3	38.5 deg C
38	300 TPD HDAN Scrubber (existing)):42-	1.37	11	1.1	50 Deg C
39	300 TPD HDAN prilling tower(Existing)	200 m	10 E	2	1.2	50 Deg C
40	40 TPH boiler (Existing)	Natural gas / FO- 73920 sm3/day or 49 MTPD		86 (Common stack for 40 TPH and 15 TPH boiler)	134	180 Deg C
41	15 TPH boiler(Existing)	Natural gas / FO - 28800 sm3/day or 26 MTPD	मुझा ^क जुड़ी	86 (Common stack for 40 TPH and 15 TPH boiler)	1.8	180 Deg C
42	Pastillator 1	0	<u> </u>	8	0.152	52 Deg C
43	Pastillator 2			8	0.152	52 Deg C
44	Batch and feed tank(Existing)	vern	MAF	10	0.152	55 Deg C
45	DG set 1 x 500 KVA (Existing)	Diesel	-	4.5	0.254	150 Deg C
46	DG set 1 x 500 KVA (existing)	Diesel	26	4.5	0.254	112 Deg C
47	DG set - 1000 KVA x 1 No (Existing)	Diesel	u O	6.5	0.254	183 Deg C
48	DG set - 1000 KVA x 1 Nos (Existing)	Diesel		6.5	0.254	183 Deg C
49	DG set - 200 KVA (Existing)	Diesel		3	0.152	88 Deg C
50	DG set - 1500 KVA (Existing)	Diesel		6.5	0.152	170 Deg C
51	DG set - 1010 KVA (Existing)	Diesel	-1	30	0.152	176 Deg C
52	DG set - 750 KVA (Existing)	Diesel		6.32	0.203	156 Deg C

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53	Process stack 1 (Existing)			60	2.8	45 Deg C
54	Process stack 2 (Existing)	-		60	2.8	45 Deg C
55	Boiler 36 TPH (Existing)	Coal – 166 TPD		66 (common stack for 36 TPH and 70 TPH boiler)	1.9	140
56	Boiler 70 TPH (Existing)	Coal - 320 TPD	र्थिका धिका	66 (common stack for 36 TPH and 70 TPH boiler)	1.9	140
57	Flare (NH3) (existing)	J.45.	37	50	0.254	
58	Flare (NH3 storage) (existing)	- 3	200	40	0.254	
59	Flare (IPA) (Existing)		2 A	66	0.584	
60	Flare (IPA) (Proposed)	<u>لالام (</u> ك	7.J.		H	
61	DG set (capacity- 200 KVA) (Proposed)	Diesel- 200 Lit/ Day		3	0.152	88 Deg C

32.Details of Fuel to be used

Serial Number	Type of Fuel	Existing	Proposed	Total
1	Natural gas (Ammonia primary reformer)	94218.5 sm3/day	0	94218.5 sm3/day
2	Natural gas / naphtha (Boiler A & B)	32400 sm3/day or 50 MTPD each	0	32400 sm3/day or 50 MTPD each
3	Natural gas / naphtha (Boiler A & B)	32400 sm3/day or 50 MTPD each	0	32400 sm3/day or 50 MTPD each
4	Natural gas (Methanol primary reformer)	60150 sm3/day	0	60150 sm3/day
5	Natural gas (Boiler C standby)	12600 sm3/day	0	12600 sm3/day
6	Natural gas or FO (Boiler D standby)	54000 sm3/day or 40 MTPD	0	54000 sm3/day or 40 MTPD
7	Natural Gas (CES - A engine)	30750 sm3/day	0	30750 sm3/day
8	Natural Gas (CES - B engine)	30750 sm3/day	0	30750 sm3/day
9	Natural Gas (Turbine 1)	37120 sm3/day	0	37120 sm3/day
10	Natural gas or naphtha (HRSG 1)	19584 sm3/day or 30 MTPD	0	19584 sm3/day or 30 MTPD
11	Natural Gas (Turbine 2)	37120 sm3/day	0	37120 sm3/day
12	Natural gas or naphtha (HRSG 2)	19584 sm3/day or 30 MTPD	0	19584 sm3/day or 30 MTPD
13	Natural Gas (Turbine 3)	42888 sm3/day	0	42888 sm3/day
14	Natural Gas (Turbine 4)	42888 sm3/day	0	42888 sm3/day
15	Natural Gas (Turbine 5)	45984 sm3/day	0	45984 sm3/day

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7392		m3/day Or 49 MT/Day			0	73920 sm3/day Or 49 MT/Day
2880		m3/day Or 26 MT/Day			0	28800 sm3/day Or 26 MT/Day
{	80	00 Lit/day			0	8000 Lit/day
	2	0 Lit/Hr			0	250 Lit/Hr
		66 TPD			0	166 TPD
		20 TPD			0	320 TPD
5	500	0 sm3/day	7.1		0	5000 sm3/day
	7	0	27	20	O Lit/ Day	200 Lit/ Day
al / Iı	mj	orted		U 3	Y _	
		material will be pelines	e trans	ported	by road tank	ers & Natural Gas by
				. 8	OVI	
	3	5.Energy	7	9		
Inl	ıhc	ise cogeneration	n plan	t & MS	SEDCL	,
n Inl	hc	use cogeneration	n plan	t & MS	SEDCL	
Ex	xis	ing DG set	3	\$ C	ST.	
7 1	M	स्य मुद्रा	32	TIL	A.	
41	M	VALVE	77	7		
2 1	2 Nos. of 8 MVA, 2 Nos. of 2.5 MVA					
51	15	ΚVA	8	n	I O	T
Di	ies	el				
Fuel used: Details of high tension line passing through the plot if any:						
ng b	Эy	non-convei	ntio	nal n	nethod:	
anels	3.					
		ulations &	% of	f sav	ing:	
Serial Number Energy Conservation Measures Saving %				ıg %		
1						
of	p	ollution cor	ntro	l Svs	tems	
	_		0			be installed
	_				-	
Source Existing pollution control systems SEIAA Meeting No: 165 Meeting Date: April 26, 2019			ntro	1 5		Proposed to

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Air pollution sources	Scrubber	for process mission, Cy ESP	clone separator,	flare
Water pollution sources		ETP, RO		ceramic membranes, resins, bioreactor
Hazardous waste generation	Dispo	sposal to CHWTSDF/ Authorize recycler		Disposal through authorized recycler
Budgetary	allocation	ion Capital cost:		
(Capital O&M				
38	38.Environmental Management plan Budgetary Allocation			

a) Construction phase (with Break-up):

Serial Number	Attributes	Attributes Parameter Total Cost per a	
1	Ambient Air	As per NAAQMS	1.62
2	Noise	As per NAAQMS	0.1
3	Dust control by water sprinking		

b) Operation Phase (with Break-up):

Serial Number	Component	Description	Capital cost Rs. In Lacs	Operational and Maintenance cost (Rs. in Lacs/yr)
1	Air Pollution Control & Monitoring	flare	1350	27
2	Noise Pollution Control	Acoustic DG set	125	2.5
3	Water Pollution Control & monitoring	ceramic membranes, resins, bioreactor	2600	52
4	Solid and Hazardous Waste management	Solid and Hazardous Waste management	20	1
5	Green belt development	Green belt development	312	40
6	Occupational Health & Safety	fire hydrant system, sensor	400	10
7	Other Green Initiatives	Solar Power	162	2
8	Other Green Initiatives	Energy Conservation (LED)	25	1

39. Storage of chemicals (inflamable/explosive/hazardous/toxic substances)

Description	Status	Location	Storage Capacity in MT	Maximum Quantity of Storage at any point of time in MT	Consumption / Month in MT	Source of Supply	Means of transportation
Ammonia	Existing	Within plot	16098	13000	50700	Self production / Imported	Tanker
Ammonia	Existing	Within plot	2480	3000	50700	Self production / Imported	Tanker

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DNA	Existing	Within plot	2 x 2093	2 x 1700	41063	Self production	Tanker
CNA	Existing	Within plot	3 x 175	3 x 140	0	Self production	Tanker
CNA	Existing	Within plot	2 x 289	2 x 230	0	Self production	Tanker
Methanol	Existing	Within plot	4498	3500	0	Self production	Tanker
Liquid CO2	Existing	Within plot	2 x 158	2 x 125	0	Self production	Tanker
Phosphoric acid	Existing	Within plot	2 x 3059	2 x 2450	27700	Imported	Tanker
Phosphoric acid	Existing	Within plot	2 x 3086	2 x 2500	27700	Imported	Tanker
Sulphuric acid	Existing	Within plot	585	475	11000	Local market	Tanker
Crude DIPE	Existing	Within plot	43	35	0	Self production	Tanker
Crude DIPE	Existing	Within plot	64	50	0	Self production	Tanker
Crude DIPE	Existing	Within plot	45	36	0	Self production	Tanker
DIPE (100 %)	Existing	Within plot	25	20	120	Self production	Tanker
Propylene	Existing	Within plot	3 x 500	3 x 400	7200	BPCL/GAIL/HPCL	Tanker
Propane	Existing	Within plot	500	400	ス -	Self production	Tanker
IPA	Existing	Within plot	5000	4000	L	Self production	Tanker
Off spec product	Existing	Within plot	72	56	× ×	Self production	
Azeo product	Existing	Within plot	72	56	37.	Self production	
Dry Product	Existing	Within plot	2 x 72	2 x 56	70 V	Self production	Tanker
Phosphoric acid(food grade)	Existing	Within plot	20	16	3	Imported	Tanker
Dil Phos acid tank	Existing	Within plot	100	80	[Self production	
Caustic lye	Existing	Within plot	30	24	120	Local Market	Tanker
DIPE storage tank (2 Nos)	Proposed	Within plot	2 x 60	2 x 48	世	Self production	Tanker
Heavy & light weight storage tanks (2 Nos)	Proposed	Within plot	2 x 60	2 x 48	E	Self production	Tanker
IPA offspec storage tank (One No)	Proposed	Within plot	900	720		Self production	
IPA storage tanks (Pharma or specialty grade) (2Nos)	Proposed	Within plot	2 x 260	2 x 200		Self production	Tanker
Day tank of heavy components(2Nos)	Proposed	Within plot	2 x 12	2 x 10	J	Self production	
Day tank DIPE (2 Nos)	Proposed	Within plot	2 x 22	2 x 16	-	Self-production	
	40.Any Other Information						

No Information Available OVERNMENTO Maharashtra

CRZ/ RRZ clearance obtain, if any:	Not applicable
Distance from Protected Areas / Critically Polluted areas / Eco-sensitiv areas/ inter-State boundaries	Not applicable
Category as per schedule of EIA Notification sheet	5 (e)- B
Court cases pending if any	J
Other Relevant Informations	ATO THE OFFICE
Have you previously submitted Application online on MOEF Website.	Yes
Date of online submission	10-10-2016

3. The proposal has been considered by SEIAA in its 165th meeting & decided to accord environmental clearance to the said project under the provisions of Environment Impact Assessment Notification, 2006 subject to implementation of the following terms and conditions:

Specific Conditions:

•	
I	PP to submit structural stability certificate of the exisitng buildings on site.
II	PP to prepare and implment CER plan in consultation with the District Auhtority as per OM issued by MoEF&CC dated 01.05.2018.
III	PP to include water and carbon foot print in the monitoirng of EMP.
IV	PP to ensure completion of Zero Liquid Discharge ETP for proposed expansion before applying for the Consent to Operate.
v	PP to ensure to comply with the conditions stipulated in the Office Memorandum issued by MoEF&CC dated 9th August, 2018.
VI	PP to submit CER plan to District Collector and submit the acknowledgement to Member Secretary, SEIAA.

General Conditions:

I	(i)PP to achieve Zero Liquid Discharge; PP shall ensure that there is no increase in the effluent load to CETP.
II	No additional land shall be used /acquired for any activity of the project without obtaining proper permission.
III	PP to take utmost precaution for the health and safety of the people working in the unit as also for protecting the environment.
IV	Proper Housekeeping programmers shall be implemented.
V	In the event of the failure of any pollution control system adopted by the unit, the unit shall be immediately put out of operation and shall not be restarted until the desired efficiency has been achieve.
VI	A stack of adequate height based on DG set capacity shall be provided for control and dispersion of pollutant from DG set. (If applicable).
VII	A detailed scheme for rainwater harvesting shall be prepared and implemented to recharge ground water.
VIII	Arrangement shall be made that effluent and storm water does not get mixed.
IX	Periodic monitoring of ground water shall be undertaken and results analyzed to ascertain any change in the quality of water. Results shall be regularly submitted to the Maharashtra Pollution Control Board.
X	Noise level shall be maintained as per standards. For people working in the high noise area, requisite personal protective equipment like earplugs etc. shall be provided.

Shri. Anil Diggikar (Member Secretary SEIAA)

XI	The overall noise levels in and around the plant are shall be kept well within the standards by providing noise control measures including acoustic hoods, silencers, enclosures, etc. on all sources of noise generation. The ambient noise levels shall confirm to the standards prescribed under Environment (Protection) Act, 1986 Rules, 1989.
XII	Green belt shall be developed & maintained around the plant periphery. Green Belt Development shall be carried out considering CPCB guidelines including selection of plant species and in consultation with the local DFO/ Agriculture Dept.
XIII	Adequate safety measures shall be provided to limit the risk zone within the plant boundary, in case of an accident. Leak detection devices shall also be installed at strategic places for early detection and warning.
XIV	Occupational health surveillance of the workers shall be done on a regular basis and record maintained as per Factories Act.
XV	(The company shall make the arrangement for protection of possible fire hazards during manufacturing process in material handling.
XVI	The project authorities must strictly comply with the rules and regulations with regard to handling and disposal of hazardous wastes in accordance with the Hazardous Waste (Management and Handling) Rules, 2003 (amended). Authorization from the MPCB shall be obtained for collections/treatment/storage/disposal of hazardous wastes.
XVII	Regular mock drills for the on-site emergency management plan shall be carried out. Implementation of changes / improvements required, if any, in the on-site management plan shall be ensured.
XVIII	A separate environment management cell with qualified staff shall be set up for implementation of the stipulated environmental safeguards.
XIX	Separate funds shall be allocated for implementation of environmental protection measures/EMP along with item-wise breaks-up. These cost shall be included as part of the project cost. The funds earmarked for the environment protection measures shall not be diverted for other purposes and year-wise expenditure should reported to the MPCB & this department
XX	The project management shall advertise at least in two local newspapers widely circulated in the region around the project, one of which shall be in the marathi language of the local concerned within seven days of issue of this letter, informing that the project has been accorded environmental clearance and copies of clearance letter are available with the Maharashtra Pollution Control Board and may also be seen at Website at http://ec.maharashtra.gov.in
XXI	Project management should submit half yearly compliance reports in respect of the stipulated prior environment clearance terms and conditions in hard & soft copies to the MPCB & this department, on 1st June & 1st December of each calendar year.
XXII	A copy of the clearance letter shall be sent by proponent to the concerned Municipal Corporation and the local NGO, if any, from whom suggestions/representations, if any, were received while processing the proposal. The clearance letter shall also be put on the website of the Company by the proponent.
XXIII	The proponent shall upload the status of compliance of the stipulated EC conditions, including results of monitored data on their website and shall update the same periodically. It shall simultaneously be sent to the Regional Office of MoEF, the respective Zonal Office of CPCB and the SPCB. The criteria pollutant levels namely; SPM, RSPM. SO2, NOx (ambient levels as well as stack emissions) or critical sectoral parameters, indicated for the project shall be monitored and displayed at a convenient location near the main gate of the company in the public domain.
XXIV	The project proponent shall also submit six monthly reports on the status of compliance of the stipulated EC conditions including results of monitored data (both in hard copies as well as by e-mail) to the respective Regional Office of MoEF, the respective Zonal Office of CPCB and the SPCB.
XXV	The environmental statement for each financial year ending 31st March in Form-V as is mandated to be submitted by the project proponent to the concerned State Pollution Control Board as prescribed under the Environment (Protection) Rules, 1986, as amended subsequently, shall also be put on the website of the company along with the status of compliance of EC conditions and shall also be sent to the respective Regional Offices of MoEF by e-mail.

- 4. The environmental clearance is being issued without prejudice to the action initiated under EP Act or any court case pending in the court of law and it does not mean that project proponent has not violated any environmental laws in the past and whatever decision under EP Act or of the Hon'ble court will be binding on the project proponent. Hence this clearance does not give immunity to the project proponent in the case filed against him, if any or action initiated under EP Act.
- 5. In case of submission of false document and non-compliance of stipulated conditions, Authority/ Environment Department will revoke or suspend the Environment clearance without any intimation and initiate appropriate legal action under Environmental Protection Act, 1986.
- 6. The Environment department reserves the right to add any stringent condition or to revoke the clearance if conditions stipulated are not implemented to the satisfaction of the department or for that matter, for any other administrative reason.
- 7. Validity of Environment Clearance: The environmental clearance accorded shall be valid as per EIA Notification, 2006, and amendments by MoEF&CC Notification dated 29th April, 2015.
- 8. In case of any deviation or alteration in the project proposed from those submitted to this department for clearance, a fresh reference should be made to the department to assess the adequacy of the condition(s) imposed and to incorporate additional environmental protection measures required, if any.
- 9. The above stipulations would be enforced among others under the Water (Prevention and Control of Pollution) Act, 1974, the Air (Prevention and Control of Pollution) Act, 1981, the Environment (Protection) Act, 1986 and rules there under, Hazardous Wastes (Management and Handling) Rules, 1989 and its amendments, the public Liability Insurance Act, 1991 and its amendments.
- 10. Any appeal against this Environment clearance shall lie with the National Green Tribunal (Western Zone Bench, Pune), New Administrative Building, 1stFloor, D-, Wing, Opposite Council Hall, Pune, if preferred, within 30 days as prescribed under Section 16 of the National Green Tribunal Act, 2010.

Shri. Anil Diggikar (Member Secretary SEIAA)

Copy to:

- 1. SECRETARY MOEF & CC
- 2. IA- DIVISION MOEF & CC
- 3. MEMBER SECRETARY MAHARASHTRA POLLUTION CONTROL BOARD MUMBAI
- 4. REGIONAL OFFICE MOEF & CC NAGPUR
- 5. REGIONAL OFFICE MPCB RAIGAD
- 6. REGIONAL OFFICE MIDC RAIGAD
- 7. MAHARASHTRA STATE ELECTRICITY DISTRIBUTION CO. LTD
- 8. COLLECTOR OFFICE RAIGAD

Maharashtra

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